UCH 1201 Principles of Chemical Engineering Humidification

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Contents

Humidity & saturation.



Outcome

 To compare the cooling process of water by contacting with air.



Indirect Contact — Heat Exchanger



$$(m \mathcal{C}_P \Delta T)_{ ext{water}} = (m \mathcal{C}_P \Delta T)_{ ext{air}}$$

For cooling of cooling-water with air in a heat exchanger, i.e., by indirect contacting of water with air, from energy balance, we can prove that 4.2 kg of air is needed for for 1 kg of water.

Density of water = 1000 kg/m^3 Density of air $\approx 1 \text{ kg/m}^3$ Air being lighter, we need to circulate a large volume of air — 4200 ltr of air per ltr of water.

Direct Contact — Cooling Tower



Cooling of Cooling Water Direct Contact — Cooling Tower (contd..)

For the entry and exit conditions, kg of water vapor per kg of dry air, are obtained from the definition of absolute humidity (H_a) , given as:

$$H_a = \frac{\text{mass of water vapor}}{\text{mass of dry air}} = \frac{n_W}{n_A} \frac{M_W}{M_A} = \frac{P_W}{P - P_W} \frac{M_W}{M_A} \quad \frac{\text{kg vapor}}{\text{kg dry air}}$$

where P_W is partial pressure of water vapor; and, P is total pressure. M_W, M_A are molecular weight of water and air respectively.



Direct Contact — Cooling Tower (contd..)

Vapor pressure of water (from table of data):

At $30^{\circ}\mathrm{C}:~31.8$ mm Hg At $45^{\circ}\mathrm{C}:~71.9$ mm Hg

From the definition of relative humidity (RH), we have

$$\mathsf{RH} = \frac{P_W}{P_W^{\mathsf{sat}}}$$

Hence,

inlet air : 30°C, 60% RH $P_W = 0.6 \times 31.8 = 19.08 \text{ mm Hg}$ exit air : 45°C, 90% RH $P_W = 0.9 \times 71.9 = 64.71 \text{ mm Hg}$



Cooling of Cooling Water Direct Contact — Cooling Tower (contd..)

The amount of water vapor in the inlet and exit are:

$$\frac{19.08}{760 - 19.08} \times \frac{18}{29} = 0.016 \text{ kg water vapor/kg dry air}$$
$$\frac{64.71}{760 - 64.71} \times \frac{18}{29} = 0.058 \text{ kg water vapor/kg dry air}$$

Amount of water vapor picked-up per kg of air = 0.058 - 0.016 = 0.042 kg.



Direct Contact — Cooling Tower (contd..)

Amount of heat removal required for 15°C drop in temperature for water = $C_P \Delta T = 4.2 \times 15 = 63 \text{ kJ/kg}$. Average latent heat of water in the range of 30–45°C= 2408 kJ/kg. Water to be vaporized for removal of 63 kJ of energy removal = $\frac{63}{2408} = 0.026 \text{ kg}$.

0.042~kg of water vapor is picked-up by 1 kg of dry air (for the entry condition of 30°C air with 60% RH, and exit condition of 45°C air with 90% RH). Hence for 0.026 kg of water, we need:

$$\frac{0.026}{0.042} = 0.62 \text{ kg of air}$$



Cooling of Cooling Water Direct Contact — Cooling Tower (contd..)

For 1 kg of water, we need to contact it with 0.62 kg of air. So as to humidify the air, water is vaporizing to air. This leads to cooling of water.

Note: there is a loss of water to the air by the amount 0.026 kg per kg of water entering i.e., 2.6%.



Comparison of Indirect Contact and Direct Contact

Summary: For the following conditions of water, and air:

Water: in = 50°C, out = 35° C

Air: in = 30°C; 60% RH, out = 45°C; 90% RH

For a reduction of $1^{\circ}\mathrm{C}$ of water, and increase of air temperature by $1^{\circ}\mathrm{C}$:

In indirect contact arrangement with heat exchanger, we need 4.2 kg of air / kg of water.

In direct contact arrangement with cooling tower, we need 0.62 kg of air / kg of water. (which is only 15% of 4.2 kg).

Hence there is a **huge** reduction in air requirement, which is simply the reduction in size of the equipment.

 "For cooling of cooling-waters, cooling-towers are much better than heat exchangers using ambient-air as the heat carrier"—Prove this statement, with simple calculation.

